

Thermally driven industrial ionic liquid absorption heat pump dryer

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Outline/Agenda



- Introduction
- Research
- Experimental Tests/Results
 - Cycle
 - System
- Conclusion

- Industrial Drying Processes

- Processes

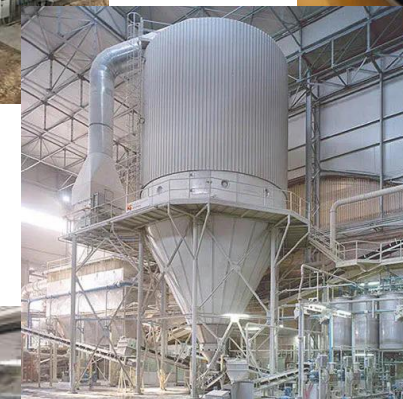
- Cement
 - Paper, Lumber
 - Textiles
 - Food
 - Pharmaceuticals

- Consumption

- Wide range of estimates
 - 10 – 20% of Industrial energy in OECD countries (972 – 1944) TWh



- Industrial Drying Processes
 - Temperatures
 - Low ($<100\text{ }^{\circ}\text{C}$)
 - Medium ($100\text{ }^{\circ}\text{C} - 400\text{ }^{\circ}\text{C}$)
 - High ($>400\text{ }^{\circ}\text{C}$)
 - Technologies
 - 50+ Types
 - Tailored to products/process
 - Quality
 - Product moisture release rate
 - Visual (discoloration, cracks, etc.)
 - Structural
- Clear incentives to reduce energy use
 - User Level – Process Economics (Cost/efficiency)
 - Societal Level – Infrastructure/Carbon footprint



- Lumber Drying
 - Low temperature – 43-82 °C (110–180 °F)
 - GHG Emissions
 - ~ 0.48% Global Total (2018)
 - 24.8 MMTCO₂e – US
 - Commercial Technologies
 - Direct Heating Dryers
 - Heat Pump Dryers



- Direct Heat Kilns ~ 90% (US – 2016)

- Single Pass

- Fuels

- Biomass, NG, other

- SMER (kg H₂O/kWh) – Wisconsin

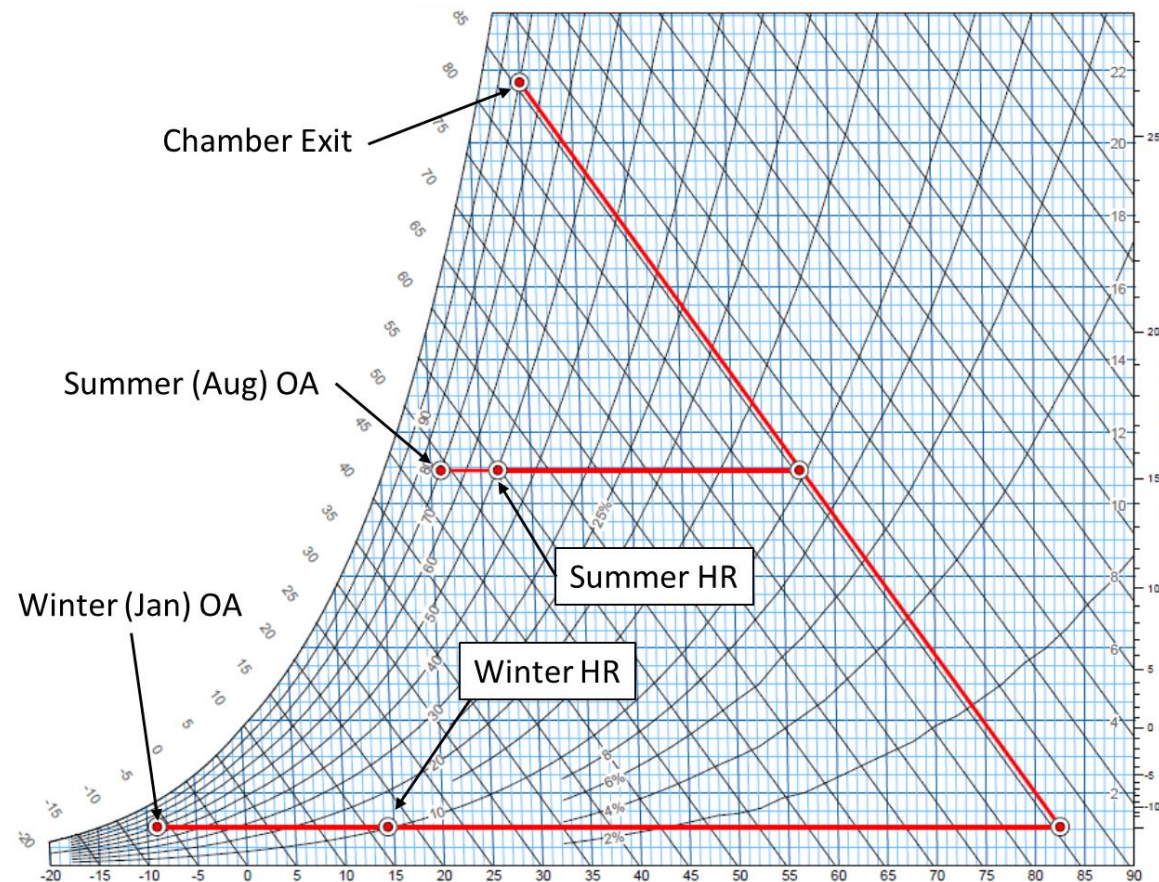
- 0.69 – 0.89

- Winter/Summer
- No Heat Recovery

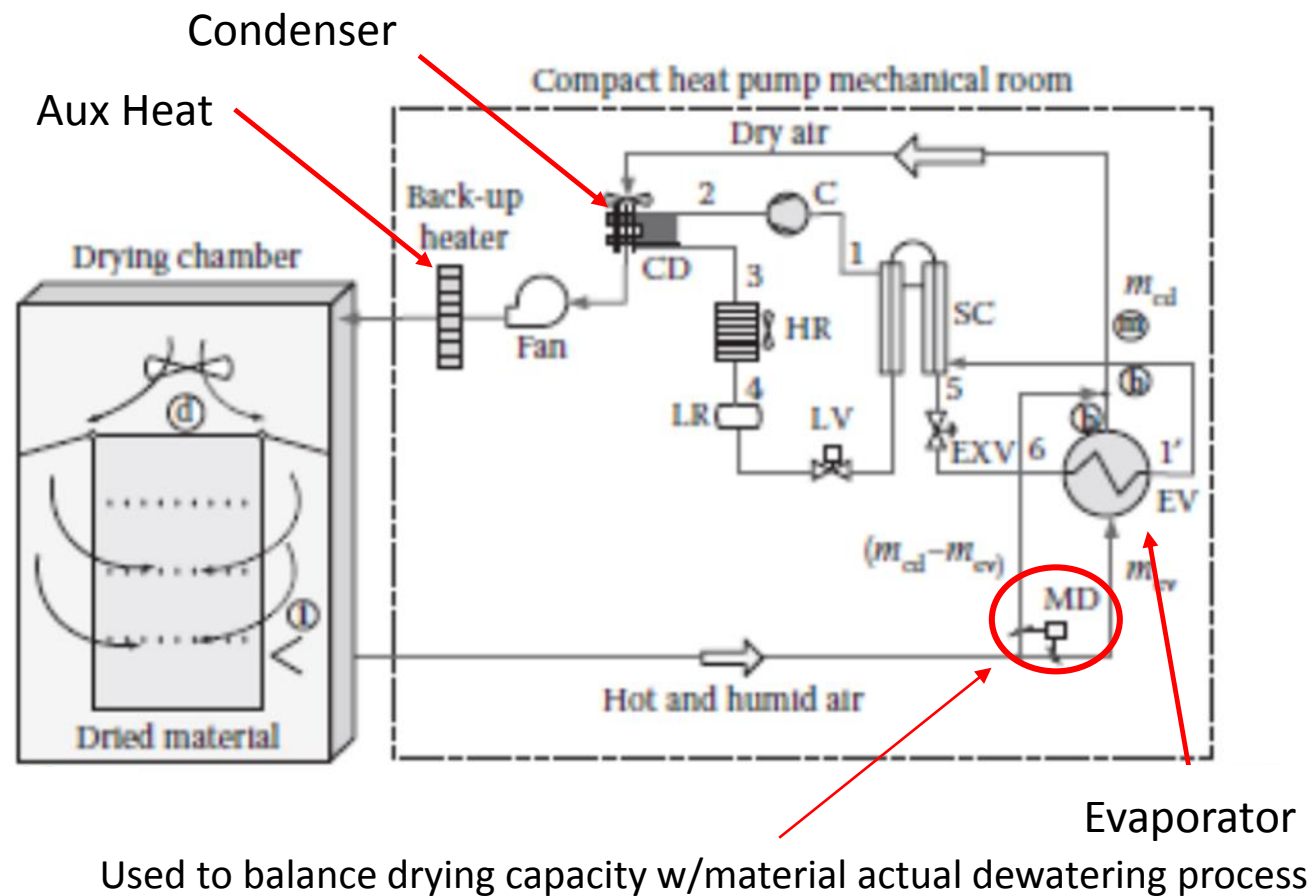
- 0.92 – 1.06

- Winter/Summer
- Heat Recovery

Climate impacts performance



- Heat Pump (HP) Kilns
 - Recirculatory
 - 40 – 60% greater efficiency
 - SMERs up to 1.4
 - Electricity driven
 - Lower Capacity Kilns (< 225,000 bf)
- Moisture Removal
 - Evaporator
 - Saturation Conditions
 - Removed as Liquid
- Reheat
 - Condenser heat recovery
 - Electric Aux Heat (as necessary)

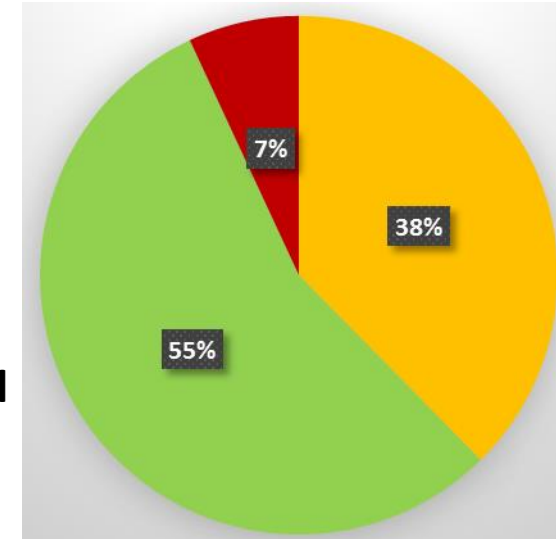


Lumber Drying – Change Barrier



Purchased Electricity (7%)

Biomass Fuel (56%)



Fossil Fuel (38%)
(coal, fuel oil,
natural gas and
other)

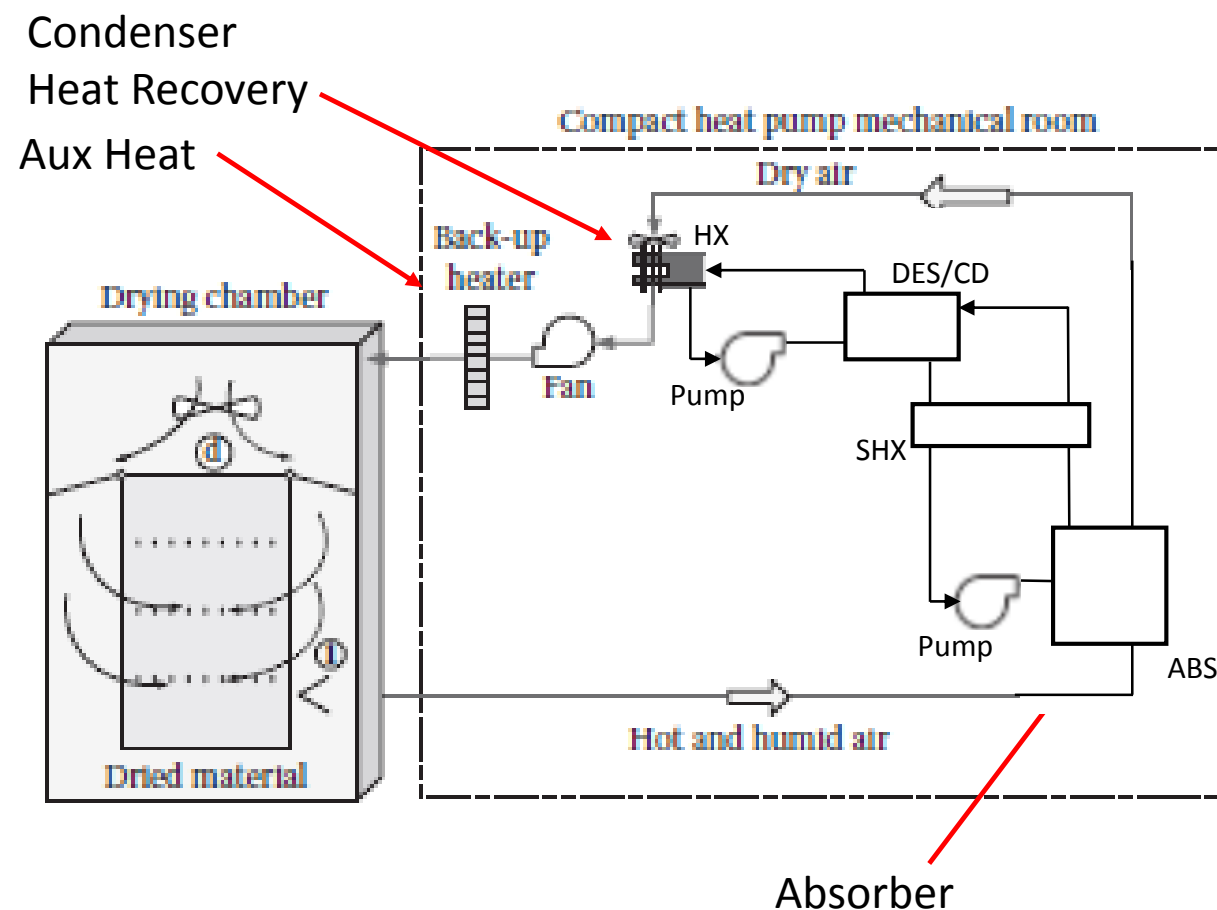
Georgia-Pacific Annual Energy Use by Source (2018)

Impact of Biomass on Process Economics

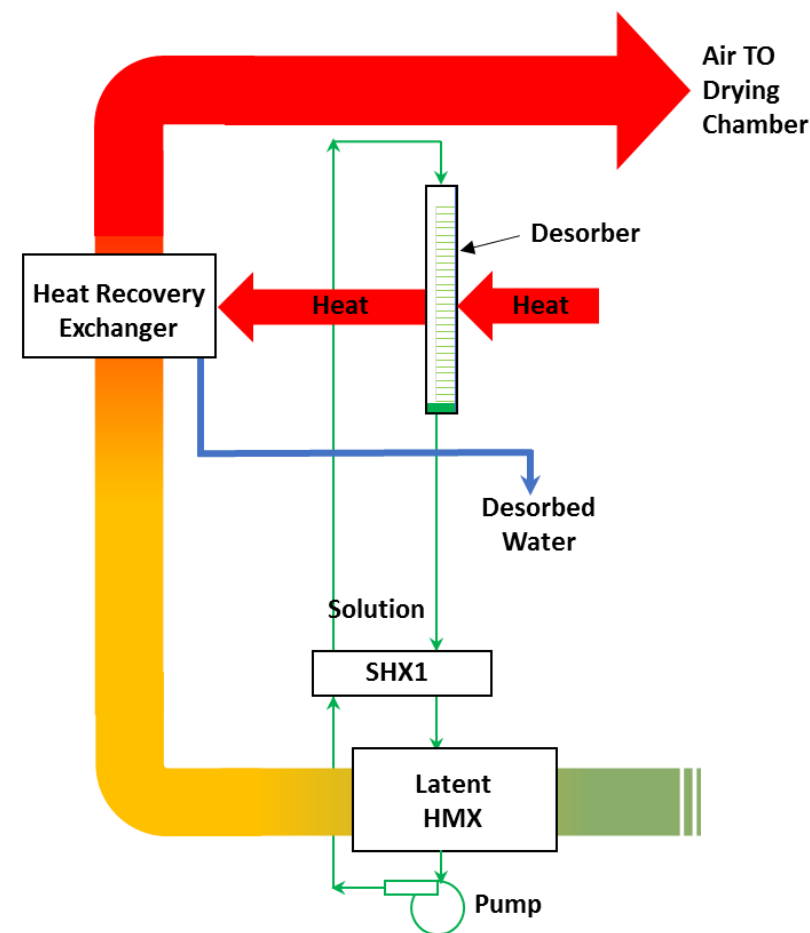
- Free byproduct
- Renewable

Introduce HP Efficiencies using Biomass

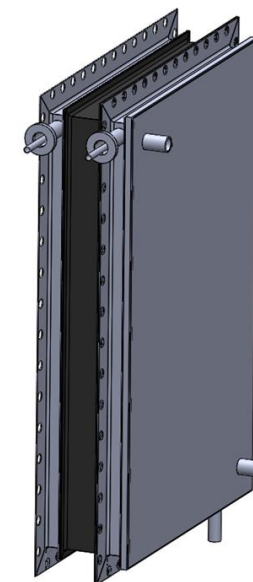
- Recirculatory Drying (AHPD)
- Heat powered (biomass)
- Moisture Removal
 - Absorber
 - Inlet Conditions
 - Removed as Vapor
- Reheat
 - Air Heated in Absorber
 - Condenser heat recovery (82 °C)
 - Aux Heat (as necessary)



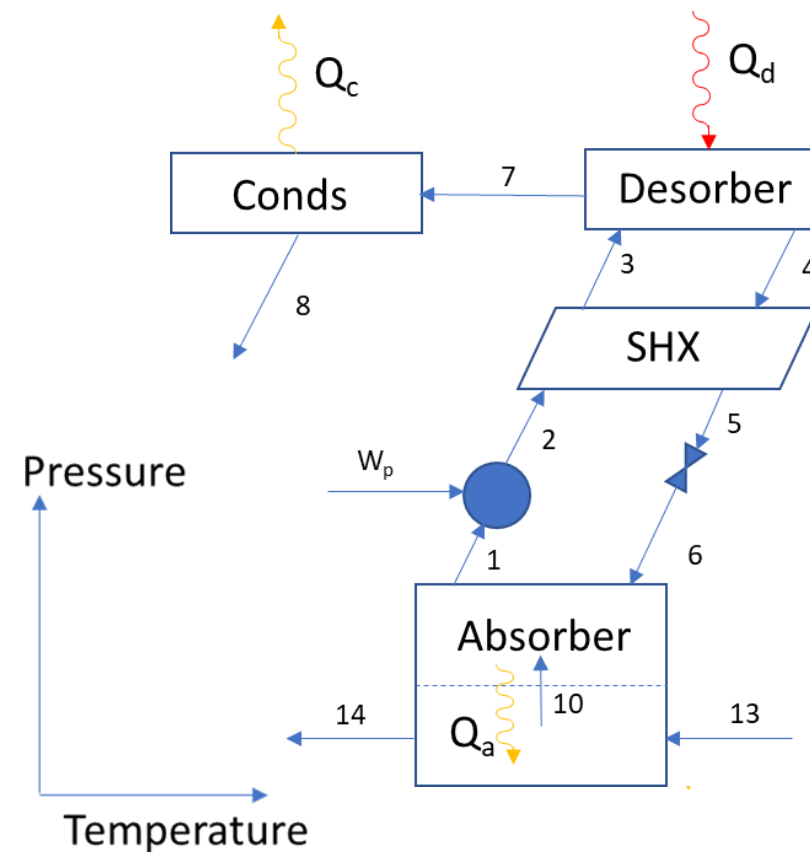
- Semi-Open Cycle
 - Introduced 2017
 - Chugh & Gluesenkamp
 - HPWH
- Characteristics
 - Single- or double-effect
 - Ionic liquid desiccant
 - Heat driven
 - Open Absorber
 - Inter-cooled
 - Adiabatic



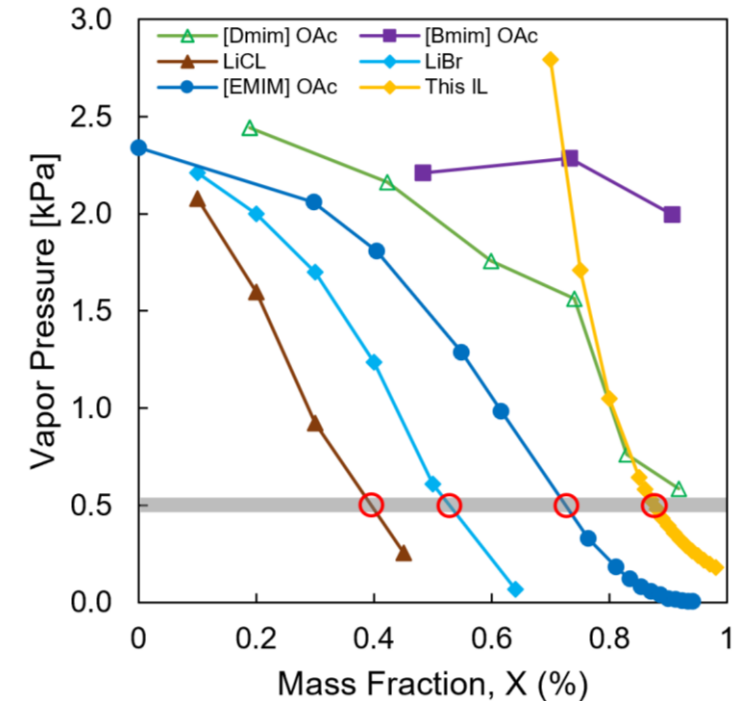
- Desorber/Condenser
 - Single effect
 - Double effect
 - Stainless Steel
 - Scalable
 - Plate & Frame Architecture
- Absorber
 - Adiabatic
 - Polymer
 - Scalable
 - Plate & Frame Architecture



- Model
 - Energy (1st Law)
 - Mass
 - Fluid Properties
 - Air – EES Property Routines
 - Ionic Liquid – Experimental
 - Absorber Properties
 - Heat and mass transfer resistances
 - Experimentally derived
 - Single & double effect
- EES Software

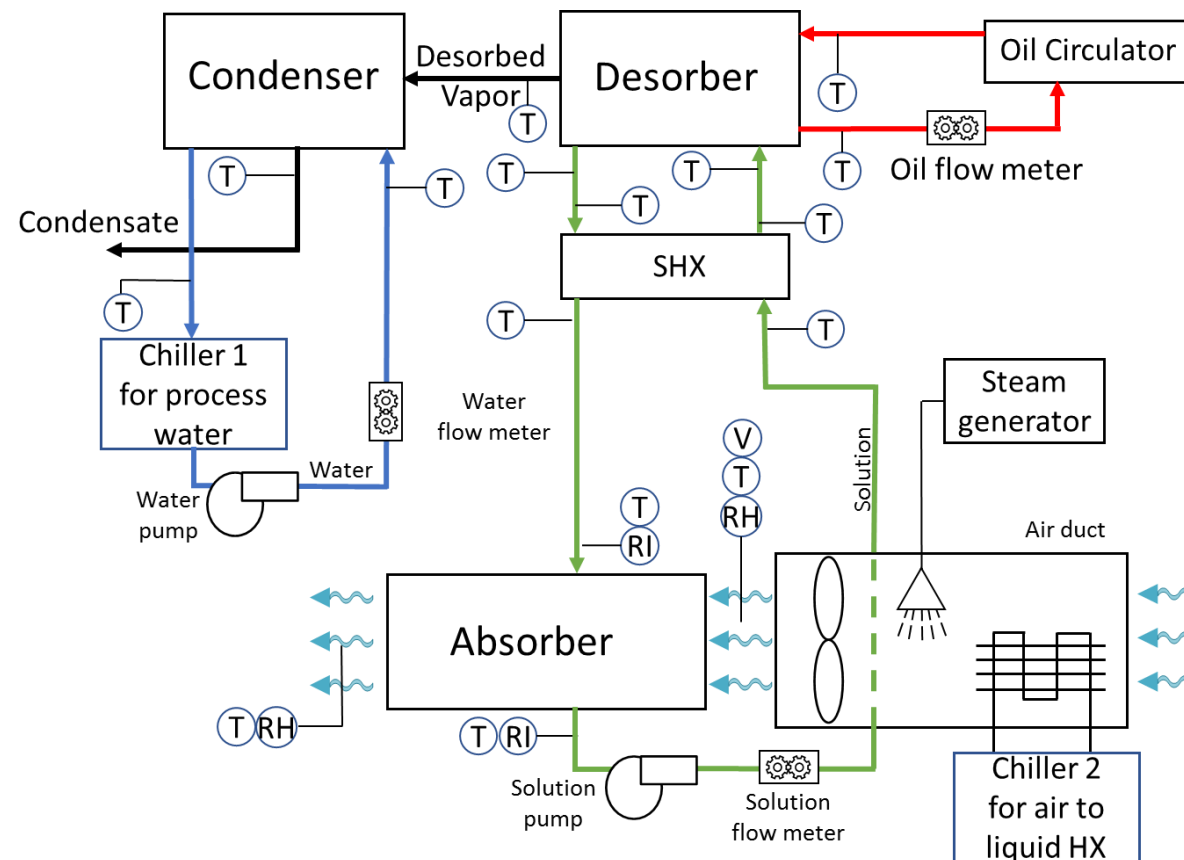


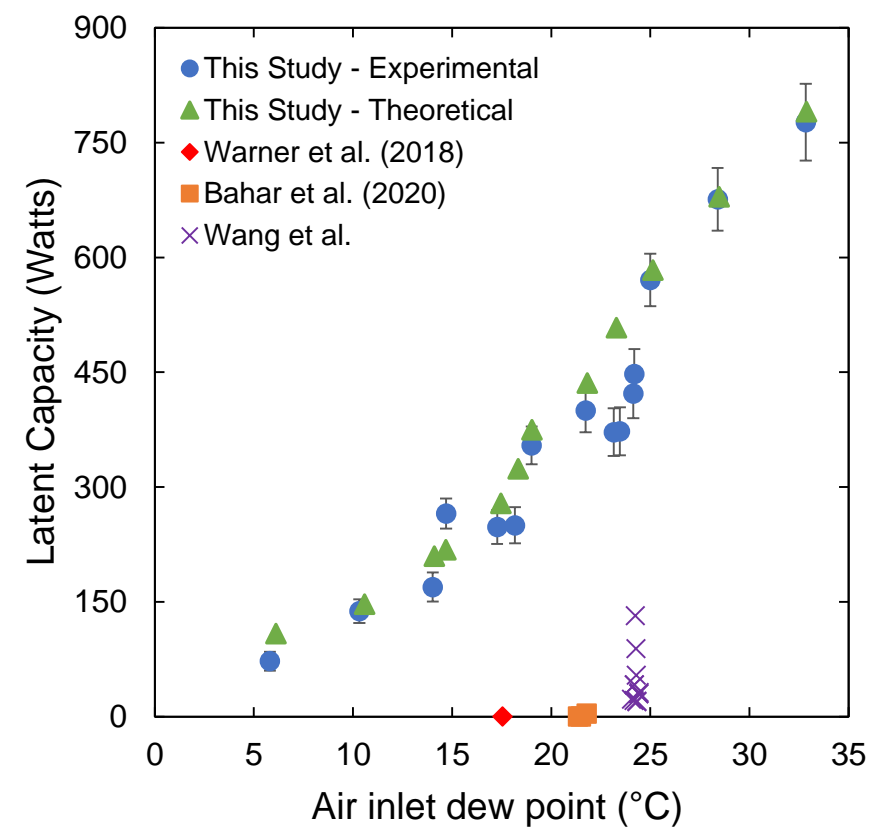
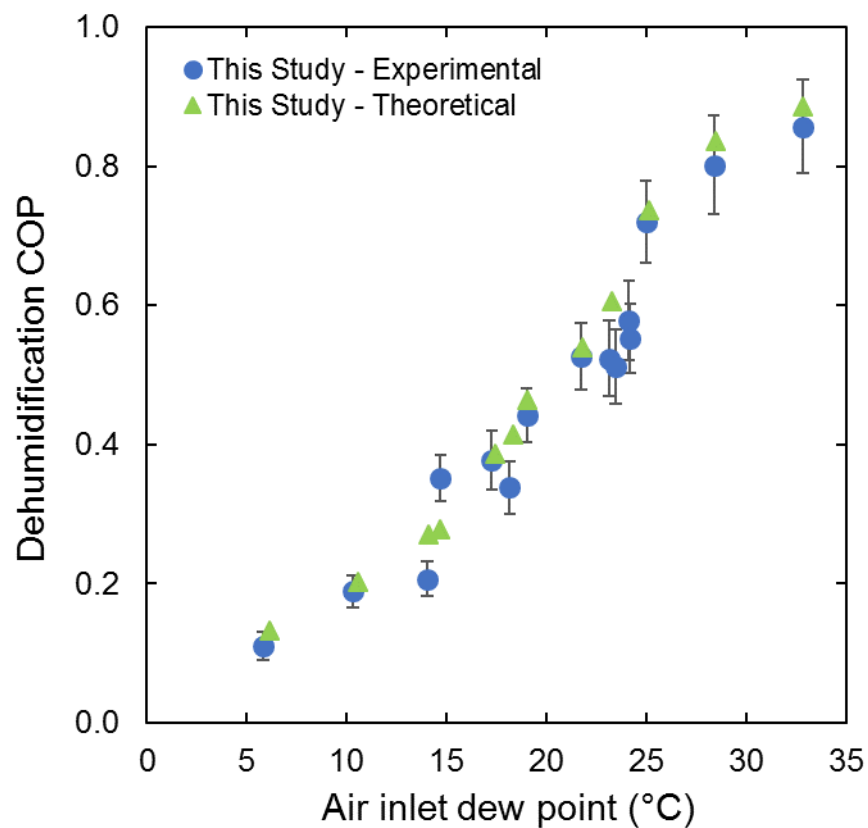
- Ionic Liquids
 - Non-crystalizing
 - Minimize control requirements
 - Increased operating envelope
 - Environmentally safe
 - < \$50/kg in quantity
- Data
 - Not available (typically)
 - Vapor Pressure
 - Thermal capacity
 - Viscosity
 - Density



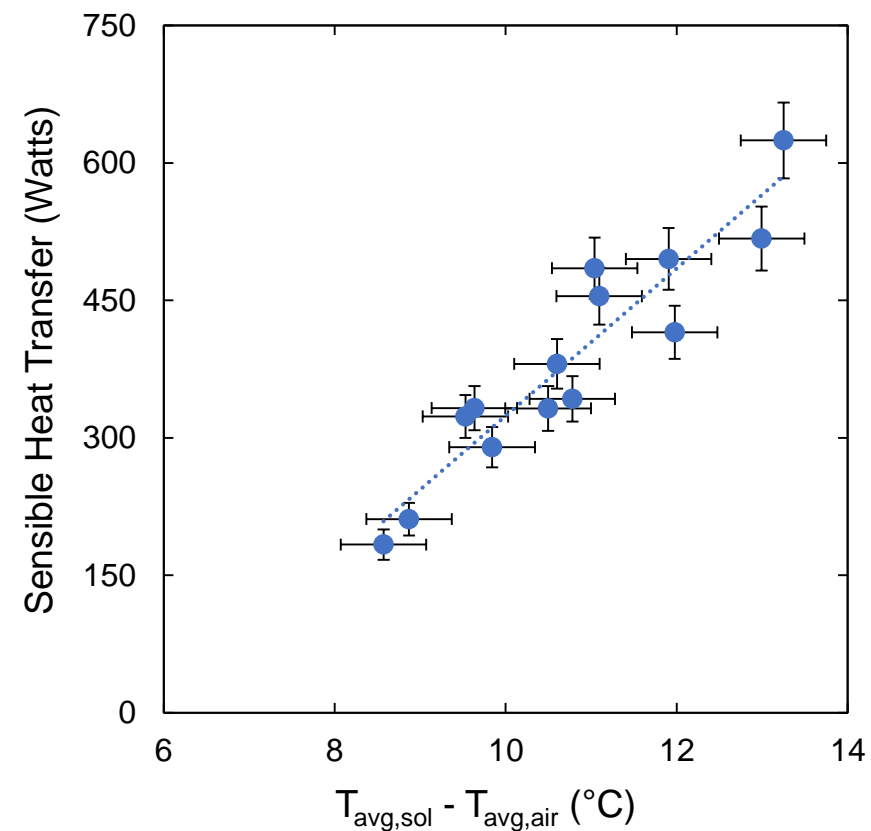
Desiccant	Viscosity (Pa-s)	Stability Limit (°C)
LiCl (20 °C, 40%)	0.0096	NA
LiBr (20°C, 53%)	0.0051	NA
[EMIM]OAc (20°C, 73%)	0.0233	~100
This IL (20°C, 87%)	0.0283	~150

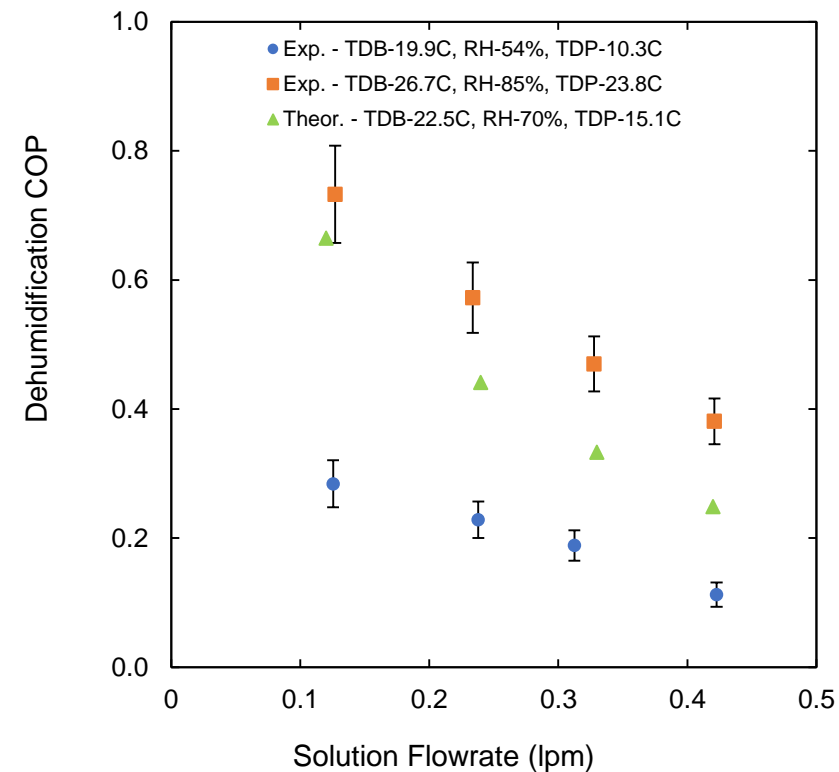
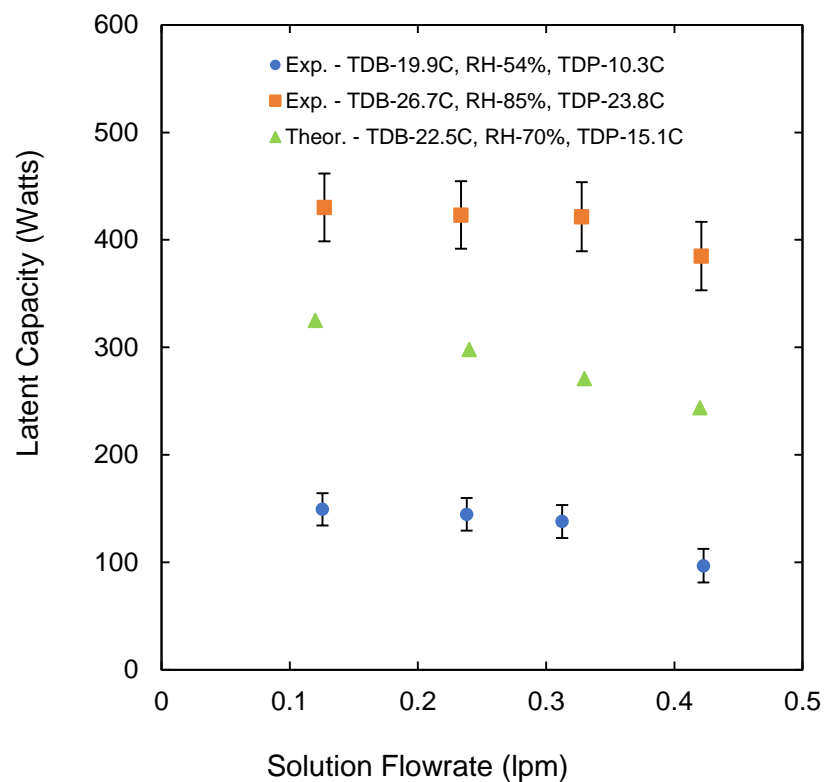
- Test System
 - Single-effect
 - ~ 1kW capacity
- Test Parameter (Consistent)
 - Solution flowrate (0.3 lpm)
 - Airflow rate (155 cfm)
 - Oil flow rate (2.85 lpm)
 - Oil inlet temp (148 °C)
- Inlet Conditions
 - $T_{dp} \sim 5 - 32 \text{ }^{\circ}\text{C}$

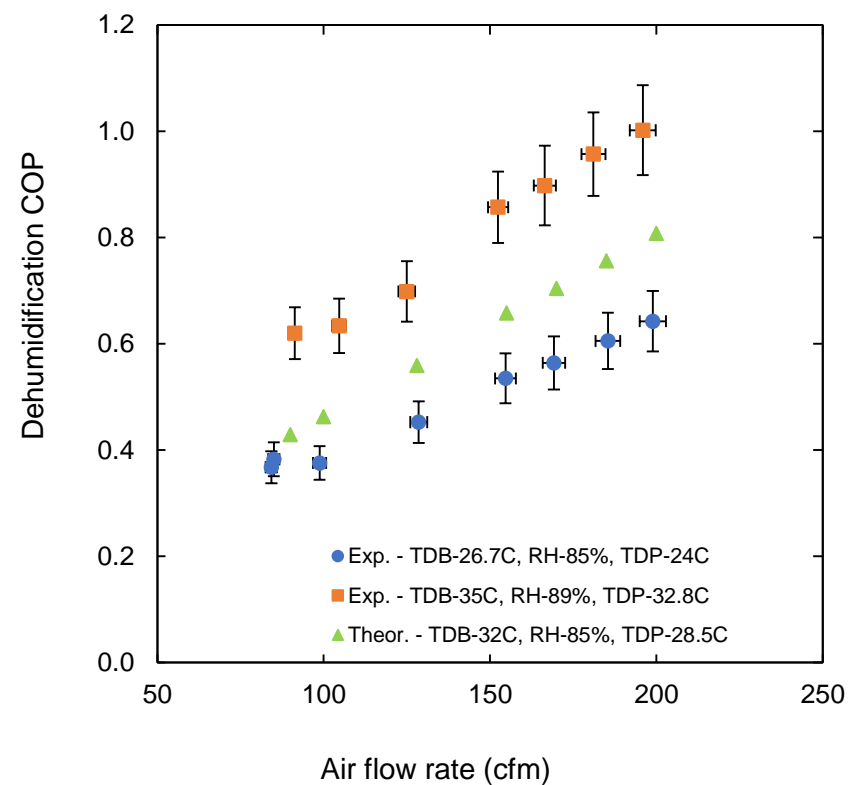
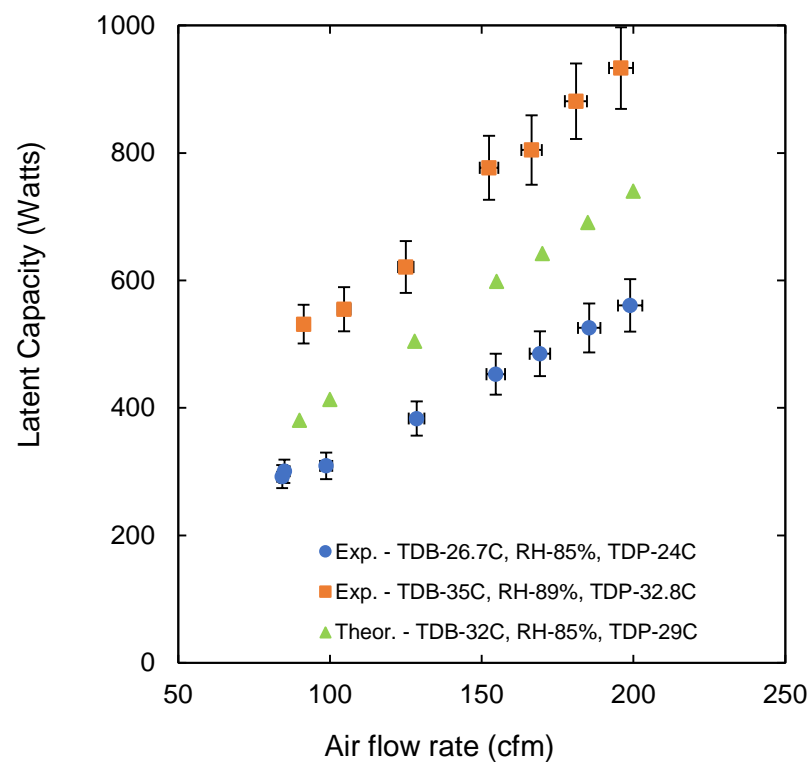




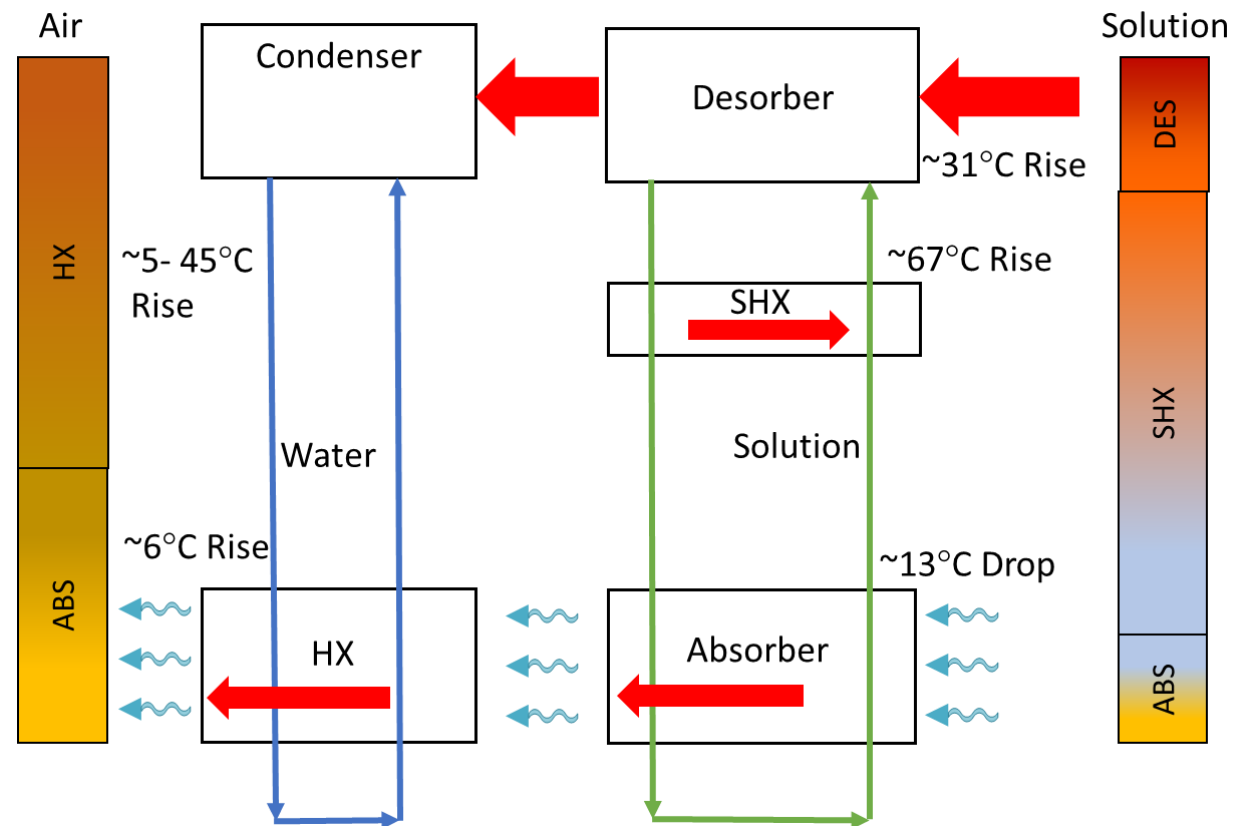
- Adiabatic Absorber
 - Process
 - Water vapor is absorbed in desiccant
 - Membrane
 - Heat of absorption is released
 - Heats process air
 - 5 – 11 °C increase



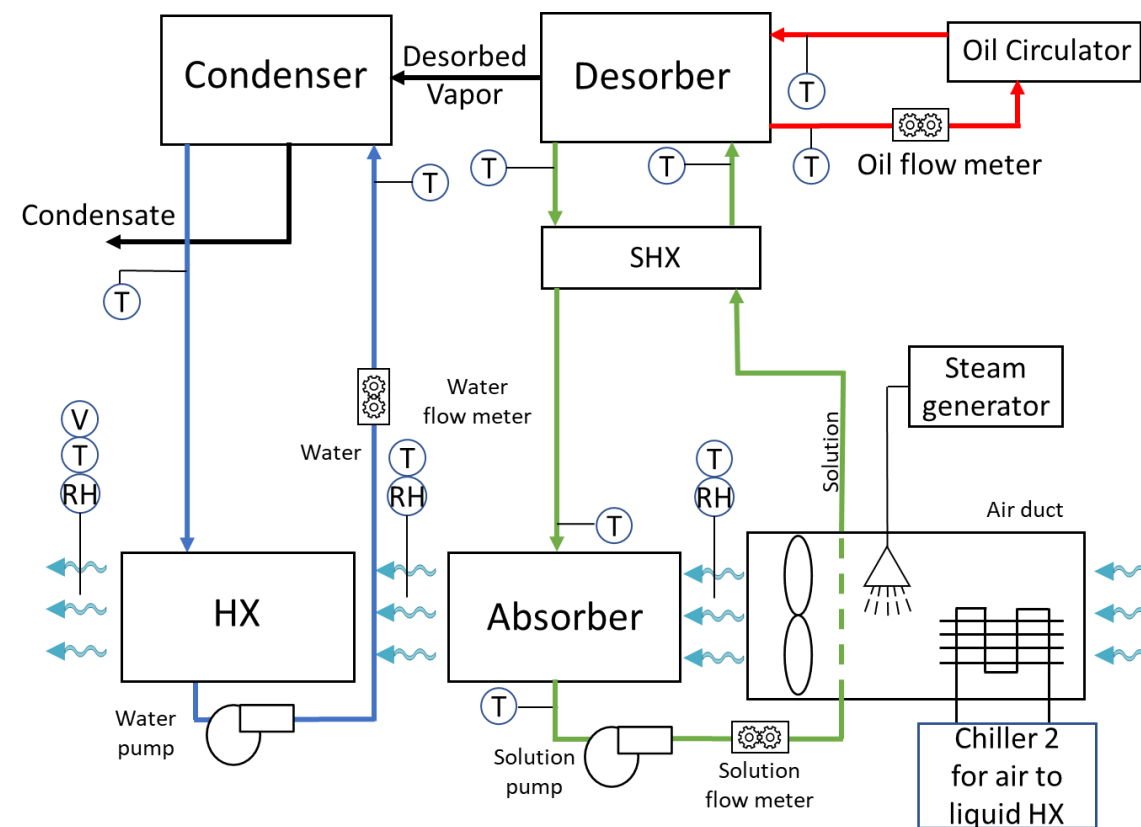




- Performance envelope
 - Single Effect
 - Double Effect
- Maximize heat recovery
 - Absorber
 - Condenser
- System characteristics
 - Capacity
 - COP



- Test System
 - Single-effect
 - Double-effect
 - ~ 1kW capacity
- Inlet Conditions
 - Lumber Drying Schedule





Experimental System

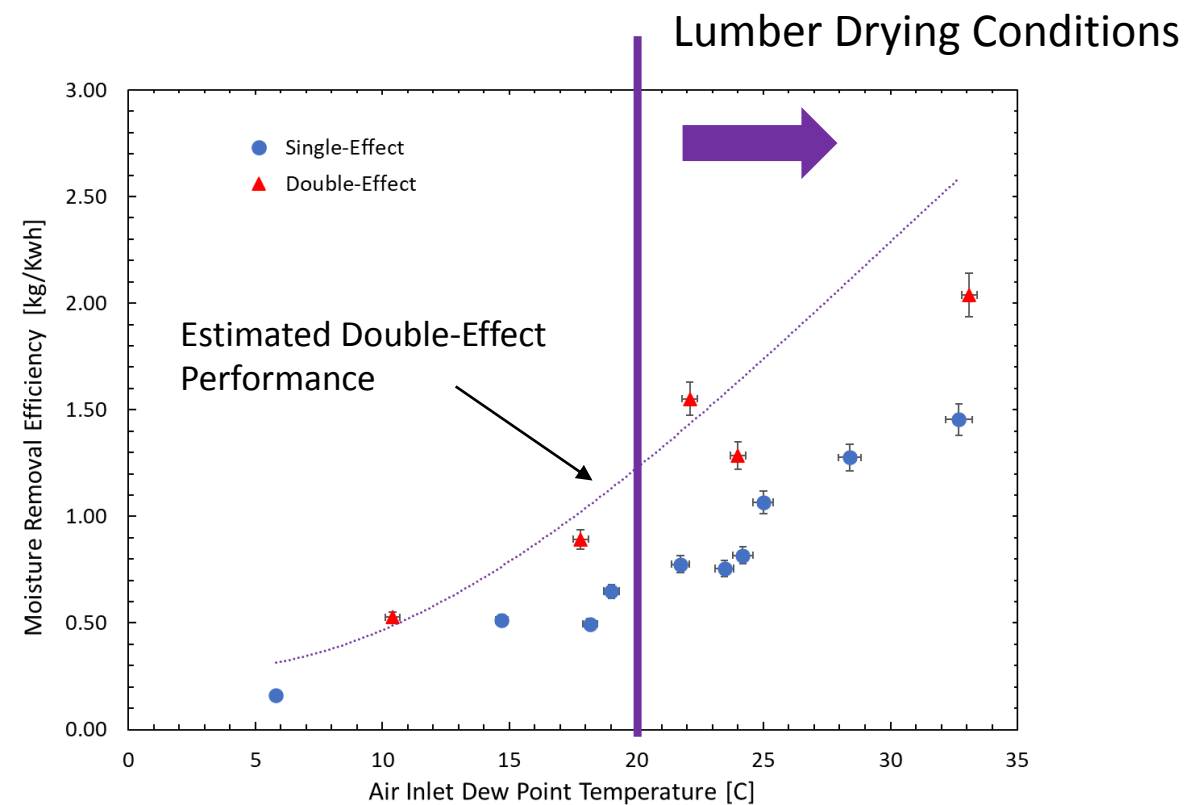
- Controls
 - Solution flow rate
 - Dehumidification capacity
 - Water flow rate
 - Condenser heat recovery
 - Condenser temp
 - Air flow rate
 - 0 – 400 cfm
- System
 - Size (consistent w/electric HP)



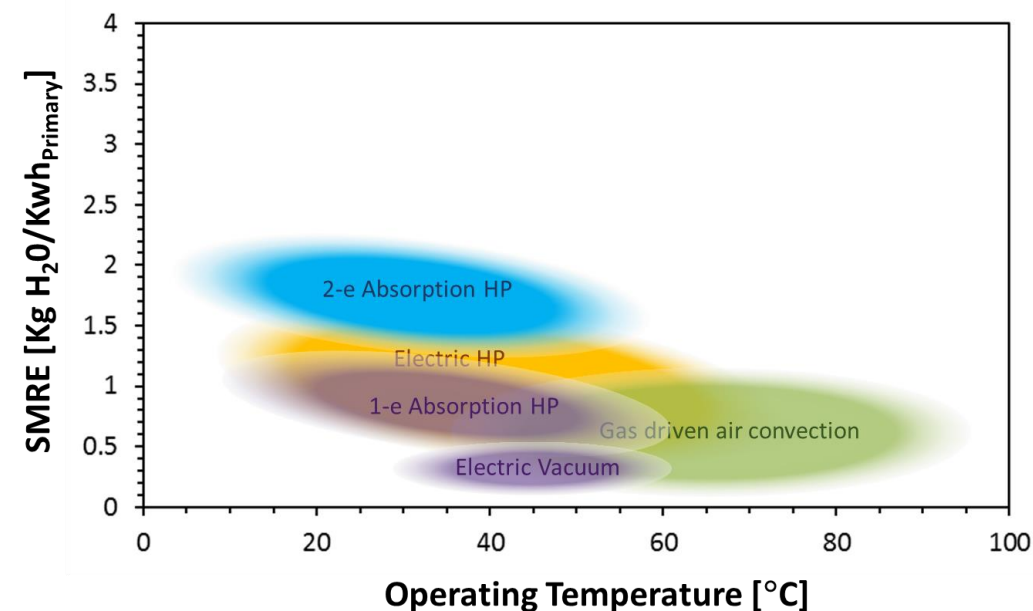
- Establishing System Settings
 - Flowrates
 - Different drying Stages
 - Single & Double effect
- In-house testing
 - Double-effect
 - Tested in Cycle test suite
 - Wide range of parameters
 - Single-effect
 - Tested in System test suite
 - Establish flowrates for lumber test conditions
- 3rd Party testing
 - GTI Energy
 - Lumber specific parameters

Stages of drying	Warm dry air supply		Warm humid air return		Air Volumetric Flowrate	Representation of Lumber moisture content (%)
	(Outlet of HP)		(Inlet of HP)			
	T _{db}	RH	T _{db}	RH		
	(°C)	%	(°C)	%	(CFM)	
1	37.8	83%	29.4	95	300	>40
2	37.8	77%	29.4	90		35 – 40
3	37.8	65%	29.4	85		30 – 35
4	40.6	46%	37.8	70		25 – 30
5	40.6	15%	37.8	50		20 – 25
6	46.1	8%	40.6	30		15 – 20

- Performance
 - Single-effect
 - w/o Optimization
 - \geq Direct Heat Kiln w/HR
 - Double-effect
 - Estimated SMER
 - 1.1 – 2.5 kg/Kwh_{primary}
- Cycle/system testing
 - June 2023



- Built an experimental demonstration unit
- Demonstrated the viability of this technology
- Absorption Heat Pump Dryer
 - Eliminate “free” fuel barrier in the lumber industry
 - Provides recirculatory dehumidification drying efficiencies for large scale lumber kilns
 - Better utilization of renewable biomass resource
 - Reducing lumber drying energy consumption and GHG emissions





Acknowledgements



- Department of Energy, Advanced Research Projects Agency Energy (ARPA-E) office,
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Thank you



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