

DEVELOPMENT OF ENERGY CALCULATION MODEL OF MULTI-SPLIT TYPE AIR-CONDITIONING SYSTEM

*Eisuke Togashi, Doctor course Student,
Shin-ichi Tanabe, Professor,
Waseda University, 3-4-1 Okubo, Shinjuku-ku, Tokyo 169-8555, JAPAN;*

Abstract: An energy calculation model for multi-split type air-conditioning system was developed. A compressor, evaporator and condenser were individually modeled to improve flexibility, since combinatorial analysis is indispensable for multi-split type air-conditioning system. With giving a specific example, procedure to estimate the parameters from the manufacturer's documentation is described. To figure out the characteristics of the multi-split type air conditioning system, sensitivity analysis was performed.

Key Words: *physical model, multi-split type air conditioning system*

1 INTRODUCTION

Recently, a great number of commercial buildings in Japan introduce all-in-one air conditioning system on a large scale. Some data shows that about 53.5% (21,221 thousand USRT in the 39,667 thousand USRT) of air-conditioning system is a type of all-in-one air conditioning system at commercial buildings in Japan. Most of them are the multi-split type air conditioning system, which is constructed of outdoor-air processing unit and more than one indoor unit. It is difficult to show the performance of multi-split type air conditioning system with characteristic formula, because characteristics of system alternate with the change of combination of outdoor-air processing unit and indoor units. Therefore optimization of multi-split type air conditioning system is difficult.

In this paper, energy calculation model of multi-split type air-conditioning system is developed to figure out the characteristics of the system. Most of parameters which is necessary to execute model is estimated from the manufacturer's documentation.

2 PHYSICAL MODEL OF REFRIGERATION CYCLE

The refrigeration cycle consists of some smaller components. In this study, the model of a compressor, an evaporator, and a condenser are all combined to calculate the refrigeration cycle. A brief calculation flow of each component is described below.

2.1 Modeling of compressor

A compression work of the compressor can be generally expressed as a function of inlet and outlet pressures as shown in equation (1). A flow rate of the refrigerant is a function of a density, and it is calculated by solving an equation of state (EOS).

2.2 Modeling of evaporator and condenser

In the evaporator, by drawing heat from an ambient air, the two-phase refrigerant could change its state to super heated. Equation (5) shows the heat balance in two-phase region, where $\Delta\theta$ is a logarithmic mean temperature difference (LMTD) expressed in equation (7). Similarly, the heat balance in the super heated region can be expressed in equation (6). Temperatures necessary to calculate the LMTD could be calculated by solving the EOS. Figure 1 shows calculation flow chart of evaporator.

The model of the condenser is almost as same as that of the evaporator.

$$W = \eta_v \text{Vol} \frac{\text{pol} - 1}{\text{pol}} P_{in} \left\{ \left(\frac{P_{out}}{P_{in}} \right)^{(\text{pol}-1)/\text{pol}} - 1 \right\} \quad (1)$$

$$W = G \Delta H_{cmp} \quad (2)$$

$$G = \eta_v \cdot \text{Vol} \cdot \rho_{in} \quad (3)$$

$$\rho_{in} = f_{EOS}(P_{in}, H_{in}) \quad (4)$$

$$\begin{aligned} Q_{sh} &= AR_{sh} K_{sh} \Delta\theta_{sh} \\ &= G_{ref} (H_{ref,out} - H_{ref,vs}) \\ &= G_{air} (H_{air,in} - H_{air,sh,out}) \end{aligned} \quad (5)$$

$$\begin{aligned} Q_{tp} &= AR_{tp} K_{tp} \Delta\theta_{tp} \\ &= G_{ref} (H_{ref,vs} - H_{ref,in}) \\ &= G_{air} (H_{air,in} - H_{air,tp,out}) \end{aligned} \quad (6)$$

$$\Delta\theta = \frac{(T_{1in} - T_{2in}) - (T_{1out} - T_{2out})}{\ln((T_{1in} - T_{2in}) / (T_{1out} - T_{2out}))} \quad (7)$$

$$1.0 = R_{sh} + R_{tp} \quad (8)$$

$$T = f_{EOS}(P, H) \quad (9)$$

$$T_{vs} = f_{EOS}(P_{vs}) \quad (10)$$

W : Compression work [kW], η_v : Volumetric efficiency [-]
 Vol : Volume [m^3], pol : Polytropic index [-]
 P : Pressure [kPa], G : Flow rate [kg/s], ρ : Density [kg/m^3]
 H : Enthalpy [kJ/kg], A : Heat transfer area [m^2]
 T : Temperature [K] R : Rate of Heat transfer area [-]
 K : Overall heat transfer coefficient [$\text{kW}/\text{m}^2\text{-K}$]
 $\Delta\theta$: Logarithmic mean temperature difference [K]
 f_{EOS} : Equation of state (EOS)

Subscripts:

ref: refrigerant, *in*: inlet state, *out*: outlet state
sh: super heated, *tp*: two-phase, *sc*: sub cooled
vs: saturated vapor state

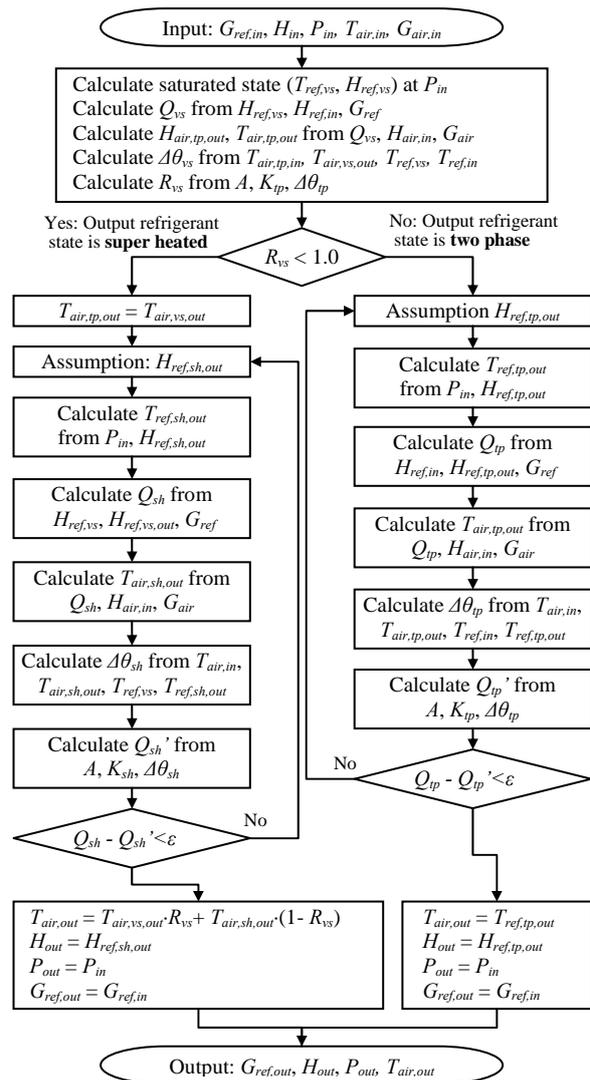


Figure 1: Calculation flow chart of the evaporator

2.3 Modeling of refrigeration cycle

With using the compressor, the evaporator, and the condenser model, refrigeration cycle model was developed.

2.3.1 Assumptions

The model is based on 5 assumptions described below.

1. Evaporating temperature is adjusted as high as possible within the limits of the heat rejection at evaporator.
2. Outlet pressure of compressor is adjusted as low as possible within the limits of the heat rejection at condenser.
3. Super heat degree is controlled at certain value with air flow at evaporator.
4. Refrigerant outlet enthalpy at condenser is controlled same value as inlet enthalpy at evaporator with air flow at condenser.
5. Revolution speed of compressor is controlled as low as possible within the limits of the heat rejection at condenser.

2.3.2 Input-output structure

Table 1 shows inputs, outputs and physical parameters of refrigerant cycle model.

Table 1; Inputs, outputs and physical parameters of refrigerant cycle model

Inputs	Outdoor air condition (Dry bulb temperature [°C], Absolute humidity [kg/kg]) Room air condition (Dry bulb temperature [°C], Absolute humidity [kg/kg]) Heat load at room [kW]
Parameters	Heat transfer area [m ²] and Overall heat transfer coefficients [kW/m ² -K] Volume of piston compression [m ³], Super heat degree [°C] Upper and lower limit of compressor outlet pressure [kPa] Upper and lower limit of evaporating temperature [°C] Upper and lower limit of compressor revolution speed [rps] Upper limit of air flow rate of HEX [kg/s]
Outputs	Compression work [kW] Electric consumption of HEX fan [kW] High and low pressure [kPa] Revolution speed of compressor [rps]

2.3.3 Calculation flow

Figure 2 shows a calculation flow chart of the refrigeration cycle. Both evaporating temperature and compressor outlet pressure are calculated iteratively.

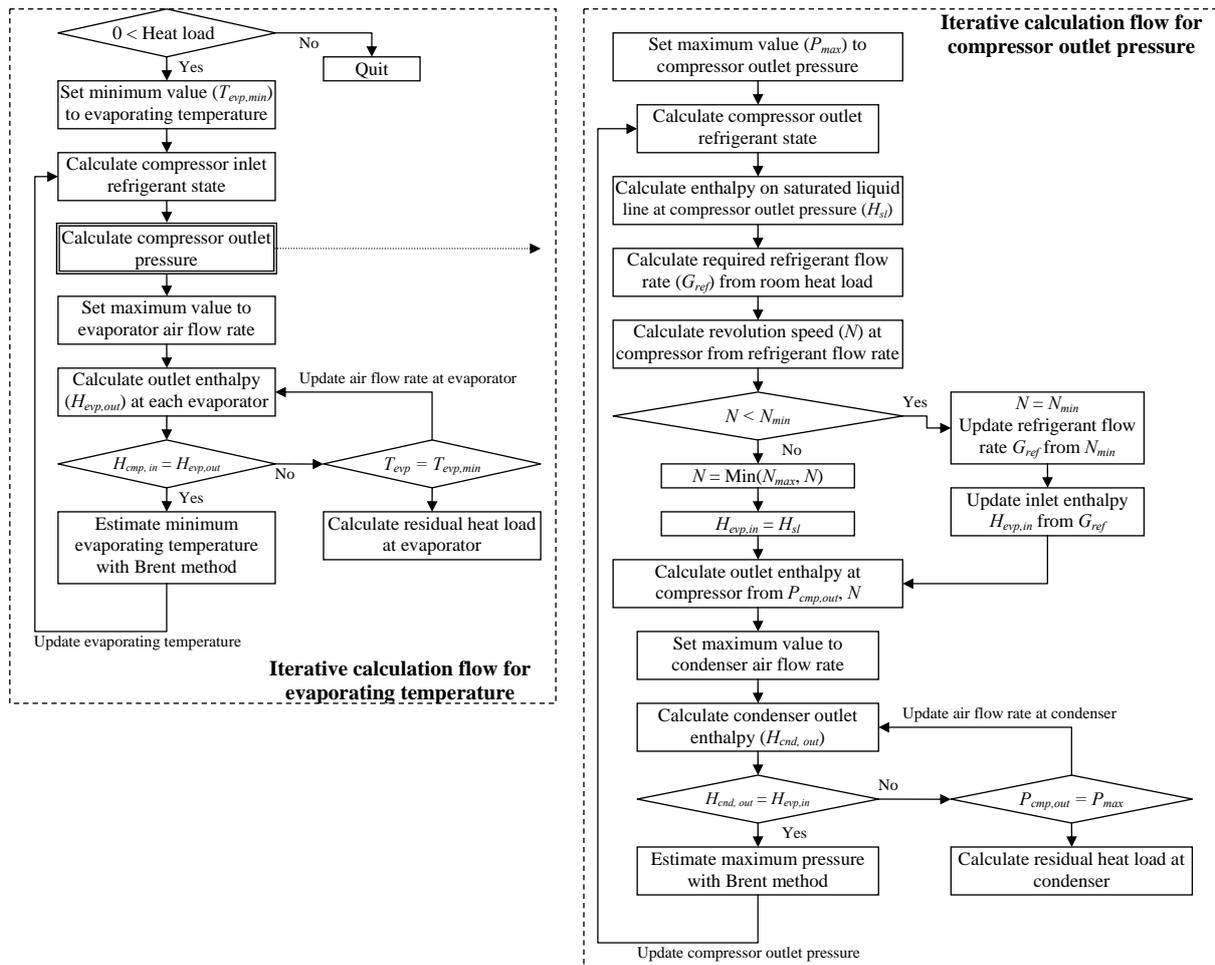


Figure 2: Calculation flow chart of the refrigeration cycle

3 PROCEDURE TO ESTIMATE THE PHYSICAL PARAMETERS

As described above, the model of refrigeration cycle needs a lot of parameters to execute simulation. Although some of parameters can be obtained from manufacturer’s web site, it’s not enough to run the model. In this section, with giving a specific example, procedure to estimate the parameters is described. Figure 3 shows an example of multi-split type air-conditioning system to estimate the parameters. 6 indoor units are connected to outdoor-air processing unit.

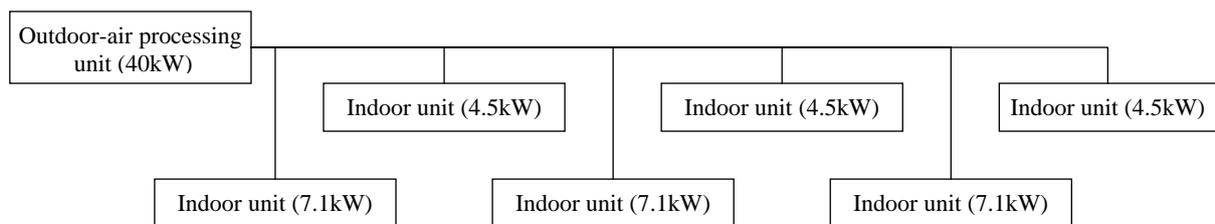


Figure 3: Sample of multi-split type air-conditioning system to estimate the parameters

3.1 Available information

The values of some physical parameters are described at documentation which can be downloaded for free from manufacturer's web site. Table 2 shows an example of the information obtained from the web site.

Table 2; Information of refrigeration components obtained from manufacturer's website

	Model	Component	Nominal performance	
Outdoor-air processing unit	RSEYP 400M	Compressor	Capacity	40 [kW]
			Electric consumption	2.0 / 4.5 / 4.5 [kW]
			Volume of piston compression	13.72 / 10.47 / 10.47 [m ³ /h]
			Revolution speed	6480 / 2900 / 2900 [rps]
		Condenser	Fan air flow rate	210 [m ³ /min]
			Fan power	0.75 [kW]
Indoor unit	FXYSP 45M	Evaporator	Fan air flow rate	11.5 [m ³ /min]
			Fan power	0.065 [kW]
			Capacity	4.5 [kW]
	FXYSP 71M	Evaporator	Fan air flow rate	21 [m ³ /min]
			Fan power	0.125 [kW]
			Capacity	7.1 [kW]
Refrigerant kind			R410A	

3.2 Estimating parameters of compressor

At the normal operating state, in refrigeration cycle of R410A, evaporating temperature is controlled to -5~5 [°C] and superheat degree takes value around 5 [°C]. Assuming that evaporating temperature as 0 [°C] and superheat degree as 5 [°C], inlet refrigerant state of compressor is determined uniquely. In this case, enthalpy, pressure, and density becomes 426.81 [kJ/kg], 798 [kPa], and 29.55 [kg/m³]. Figure 4 shows the determination of compressor inlet refrigerant state at nominal state.

Refrigerant flow rate can be calculated from compression volume and density of compressor inlet refrigerant. Assuming that volumetric efficiency is 0.95, $(13.72 + 10.47 + 10.47) \text{ [m}^3\text{/h]} / 3600 \times 29.55 \text{ [kg/m}^3\text{]} \times 0.95 = 0.27 \text{ [kg/s]}$ is a flow rate of refrigerant in this case.

From nominal capacity and refrigerant flow rate, inlet enthalpy of evaporator can be determined uniquely. In this case, $426.81 \text{ [kJ/kg]} - 40 \text{ [kW]} / 0.27 \text{ [kg/s]} = 278.7 \text{ [kJ/kg]}$.

Saturated liquid line and vertical line at evaporator inlet enthalpy intersect at one point, which shows outlet refrigerant state of condenser, 278.7 [kJ/kg] and 2830 [kPa] in this case.

Compression work can be calculated from pressure difference at compressor (Equation 1).

Using ratio of specific heat capacities in place of polytropic index, compression work is calculated to be 10.9 [kW]. Additionally, increased enthalpy at compressor can be calculated from compression work and refrigerant flow rate (Equation 2). In this case, $426.81 \text{ [kJ/kg]} + 10.9 \text{ [kW]} / 0.27 \text{ [kg/s]} = 467.18 \text{ [kJ/kg]}$ is outlet enthalpy at compressor.

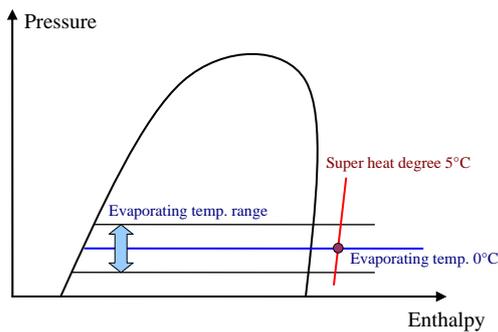


Figure 4: Determination of compressor inlet refrigerant state at nominal condition

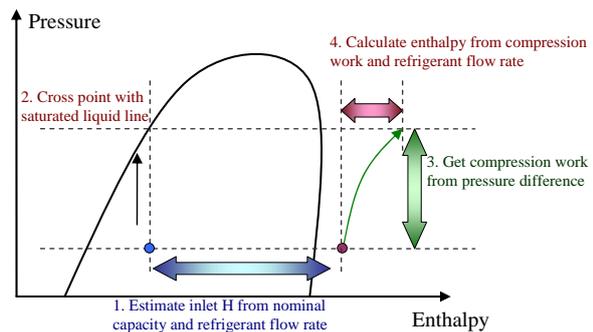


Figure 5: Determination of HEX inlet and outlet refrigerant state at nominal condition

3.3 Estimating parameters of condenser

As inlet and outlet state and flow rate of refrigerant is identified at foregoing section, heat exchanger duty at condenser can be calculated analytically. Assuming that K_{sp} equals K_{tp} , heat transfer area can be determined uniquely with solving equation (5), (6), and (7). From Japanese Industrial Standards (JIS), outdoor air dry bulb temperature to test nominal performance is 35.0 [°C]. The value of air flow rate is already obtained at section 3.1. In this case, heat transfer area is calculated to be 91.8 [m²] when $K_{sp} = K_{tp} = 0.045$ [kW/K-m²].

3.4 Estimating parameters of evaporator

Heat exchanger duty at evaporator can be obtained as the same way as condenser. However, refrigerant flow rate is determined as a function of ratio of nominal power of outdoor air processing unit to that of indoor unit. In the case of FXYSP71M, refrigerant flow rate is calculated to be 0.0479 [kg/s] = 0.27 [kg/s] × (7.1 [kW] / 40 [kW]). From Japanese Industrial Standards (JIS), indoor air state to test nominal performance is 27.0 [°CDB] and 19 [°CWB]. In this case, heat transfer area of FXYSP71M and FXYSP45M is calculated to be 8.2 [m²] and 5.4 [m²], respectively when $K_{sp} = K_{tp} = 0.045$ [kW/K-m²].

4 SENSITIVITY ANALYSIS

Using model built at foregoing section, sensitivity analysis was performed to figure out the characteristics of multi-split type air conditioning system.

4.1 Response characteristics to changes of outdoor air state

Table 3 shows the response characteristics to changes of outdoor air state. High pressure drops down since heat exchange performance increases with decline of temperature. Because heat load to solve is constant, as pressure difference at compressor and compression work decreases, COP rises from 3.4 to 3.9. Figure 6 shows system COP against out door dry bulb temperature.

Table 3; Response characteristics to changes of outdoor air state

RSEYP400M	Outdoor DB temperature	35	34	33	32	31
	Outdoor absolute humidity	0.027	0.027	0.027	0.027	0.027
	Indoor heat load	34.8	34.8	34.8	34.8	34.8
	Evaporating temperature	0.00	0.00	0.00	0.00	0.00
	System COP	2.91	2.99	3.08	3.17	3.26
	COP (no fans electric consumption)	3.40	3.52	3.64	3.77	3.91
	Compression work	10.23	9.89	9.55	9.23	8.91
	Revolution speed	96.6	95.4	94.1	92.9	91.8
	Low pressure	798.3	798.1	798.0	797.9	797.8
	High pressure	2979.0	2912.1	2844.2	2778.5	2713.6
	Refrigerant flow rate	0.242	0.238	0.235	0.232	0.229
	Compressor inlet enthalpy	428.2	428.2	428.2	428.2	428.2
	Compressor outlet enthalpy	470.6	469.7	468.8	468.0	467.1
	Condenser outlet DB temperature	45.7	44.6	43.5	42.4	41.3
	Condenser outlet absolute humidity	0.027	0.027	0.027	0.027	0.027
	condenser outlet enthalpy	284.2	282.3	280.3	278.4	276.5
heat exchange	45.0	44.7	44.3	44.0	43.7	
FXYSP71M	Indoor DB temperature	27	27	27	27	27
	Indoor absolute humidity	0.01	0.01	0.01	0.01	0.01
	Air flow rate	0.42	0.42	0.42	0.42	0.42
	Fan power	0.206	0.206	0.206	0.206	0.206
	Outlet air DB temperature	12.7	12.7	12.7	12.7	12.7
	Outlet air absolute humidity	0.009	0.009	0.009	0.009	0.009
	heat load	7.1	7.1	7.1	7.1	7.1
FXYSP45M	Indoor DB temperature	27	27	27	27	27
	Indoor absolute humidity	0.01	0.01	0.01	0.01	0.01
	Air flow rate	0.23	0.23	0.23	0.23	0.23
	Fan power	0.127	0.127	0.127	0.127	0.127
	Outlet air DB temperature	11.6	11.6	11.6	11.6	11.6
	Outlet air absolute humidity	0.008	0.008	0.008	0.008	0.008
	heat load	4.5	4.5	4.5	4.5	4.5

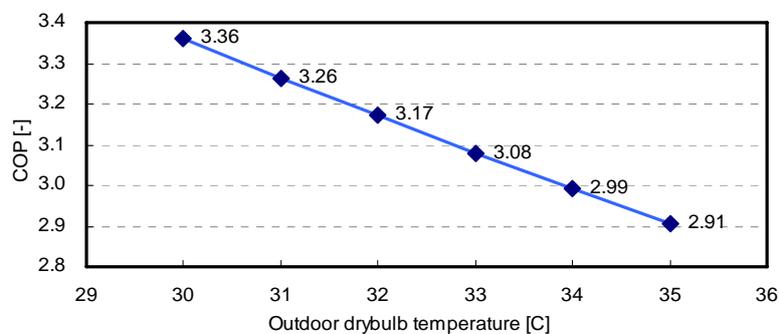


Figure 6: System COP against out door dry bulb temperature

4.2 Response characteristics to changes of evaporating temperature

Table 4 shows the response characteristics to changes of evaporating temperature. Although developed model can automatically adjust its evaporating temperature, evaporating temperature is fixed to certain value in this case study.

Since increase of evaporating temperature directly linked to increase of low pressure, pressure difference at compressor decreases. As a result, COP rises from 3.3 to 3.8 with evaporating temperature increases from -5.0 to 1.0. Figure 7 shows system COP against evaporating temperature.

Table 4; Response characteristics to changes of evaporating temperature

RSEYP400M	Outdoor DB temperature	30	30	30	30
	Outdoor absolute humidity	0.027	0.027	0.027	0.027
	Indoor heat load	27.84	27.84	27.84	27.84
	Evaporating temperature	-5.00	-3.00	-1.00	1.00
	System COP	3.29	3.47	3.65	3.83
	COP (no fans electric consumption)	3.77	4.03	4.32	4.64
	Compression work	7.39	6.91	6.44	6.00
	Revolution speed	83.6	77.8	72.5	67.7
	Low pressure	678.3	724.4	772.9	823.8
	High pressure	2485.7	2481.6	2478.6	2474.5
	Refrigerant flow rate	0.177	0.176	0.176	0.175
	Compressor inlet enthalpy	426.5	427.2	427.9	428.5
	Compressor outlet enthalpy	468.2	466.4	464.6	462.9
	Condenser outlet DB temperature	38.3	38.2	38.1	38.0
	Condenser outlet absolute humidity	0.027	0.027	0.027	0.027
	condenser outlet enthalpy	269.6	269.4	269.3	269.2
heat exchange	35.2	34.7	34.3	33.8	
FXYSP71M	Indoor DB temperature	27	27	27	27
	Indoor absolute humidity	0.010	0.010	0.010	0.010
	Air flow rate	0.13	0.15	0.17	0.21
	Fan power	0.064	0.072	0.084	0.104
	Outlet air DB temperature	-0.3	2.5	5.5	8.5
	Outlet air absolute humidity	0.004	0.005	0.006	0.007
heat load	5.68	5.68	5.68	5.68	
FXYSP45M	Indoor DB temperature	27	27	27	27
	Indoor absolute humidity	0.010	0.010	0.010	0.010
	Air flow rate	0.08	0.09	0.10	0.13
	Fan power	0.044	0.050	0.058	0.070
	Outlet air DB temperature	-0.9	1.9	4.8	7.8
	Outlet air absolute humidity	0.004	0.004	0.005	0.007
heat load	3.6	3.6	3.6	3.6	

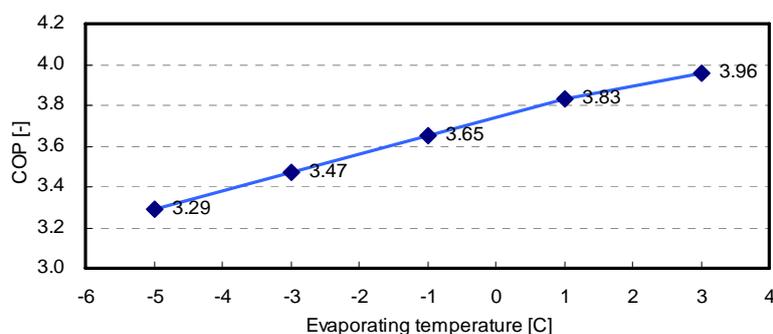


Figure 7: System COP against evaporating temperature

4.3 Response characteristics to changes of indoor heat load

Table 5 shows the response characteristics to changes of indoor heat load. With decreasing of indoor heat load, evaporating temperature and revolution speed of compressor increase and decrease respectively. Finally, evaporating temperature reach to upper limit (5 [°C] in this case) and revolution speed reach to lower limit (50 [rps] in this case). Keeping with this trend, COP curve shows single-peaked pattern. Figure 8 shows system COP against indoor heat load.

Table 5; Response characteristics to changes of indoor heat load

RSEYP400M	Outdoor DB temperature	35	35	35	35	35
	Outdoor absolute humidity	0.027	0.027	0.027	0.027	0.027
	Indoor heat load	34.8	30	25.2	20.4	15.6
	Evaporating temperature	0.0	2.5	5.0	5.0	5.0
	System COP	2.91	3.25	3.60	3.51	2.88
	COP (no fans electric consumption)	3.40	3.96	4.63	4.42	3.55
	Compression work	10.23	7.58	5.44	4.62	4.39
	Revolution speed	96.6	74.5	56.1	50.0	50.0
	Low pressure	798.3	863.5	933.2	933.2	933.2
	High pressure	2979.0	2841.9	2711.7	2593.8	2481.3
	Refrigerant flow rate	0.242	0.202	0.164	0.146	0.146
	Compressor inlet enthalpy	428.2	429.0	429.7	429.7	429.7
	Compressor outlet enthalpy	470.6	466.6	462.8	461.2	459.7
	Condenser outlet DB temperature	45.7	43.9	42.3	40.9	39.7
FXYS71M	Condenser outlet absolute humidity	0.027	0.027	0.027	0.027	0.027
	condenser outlet enthalpy	284.2	280.2	276.4	290.4	323.2
	heat exchange	45.0	37.6	30.6	25.0	20.0
	Indoor DB temperature	27	27	27	27	27
	Indoor absolute humidity	0.010	0.010	0.010	0.010	0.010
	Air flow rate	0.42	0.42	0.41	0.22	0.14
	Fan power	0.206	0.206	0.200	0.109	0.069
FXYS45M	Outlet air DB temperature	12.7	13.4	14.0	10.9	8.1
	Outlet air absolute humidity	0.009	0.010	0.010	0.008	0.007
	heat load	7.1	6.3	5.5	4.7	3.9
	Indoor DB temperature	27	27	27	27	27
	Indoor absolute humidity	0.010	0.010	0.010	0.010	0.010
	Air flow rate	0.23	0.17	0.12	0.07	0.04
	Fan power	0.127	0.093	0.069	0.037	0.020
Outlet air DB temperature	11.6	10.6	10.0	6.5	4.4	
Outlet air absolute humidity	0.008	0.008	0.008	0.006	0.005	
heat load	4.5	3.7	2.9	2.1	1.3	

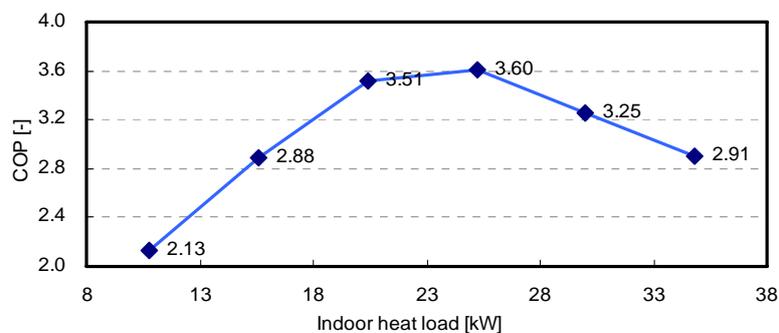


Figure 8: System COP against indoor heat load

5 CONCLUSION

In this paper, energy calculation model of multi-split type air-conditioning system was developed. With giving a specific example, procedure to estimate the parameters from the manufacturer's documentation was described. To figure out the characteristics of the multi-split type air conditioning system, sensitivity analysis was performed. Theoretical relationship between COP and outdoor dry bulb temperature, evaporating temperature, and indoor heat load was show diagrammatically.

6 ACKNOWLEDGMENT

This research was partially supported by the Ministry of Education, Science, Sports and Culture, Grant-in-Aid for Scientific Research (A), No.19206063, 2007. The authors express gratitude to Professor S. Kawai and Mr. S. Yamaguchi for valuable advices about physical model of heat pump chiller.